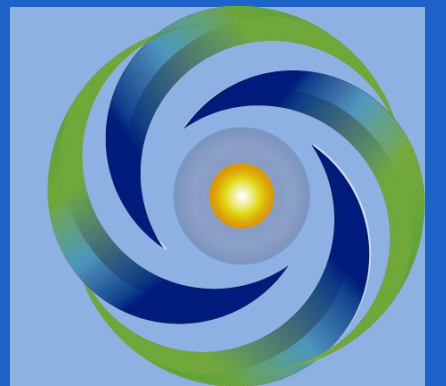


From Waste Treatment to Fuel Production: Ensuring Energy Circularity

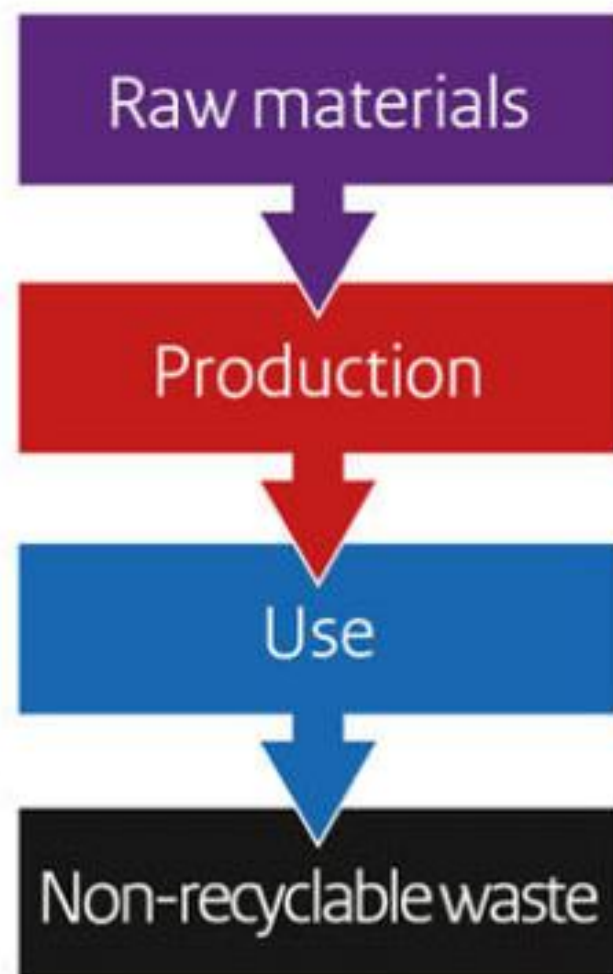
Joris W. Thybaut

Laboratory for Chemical Technology (LCT), Ghent University, Technologiepark 125,
9052, Ghent, Belgium

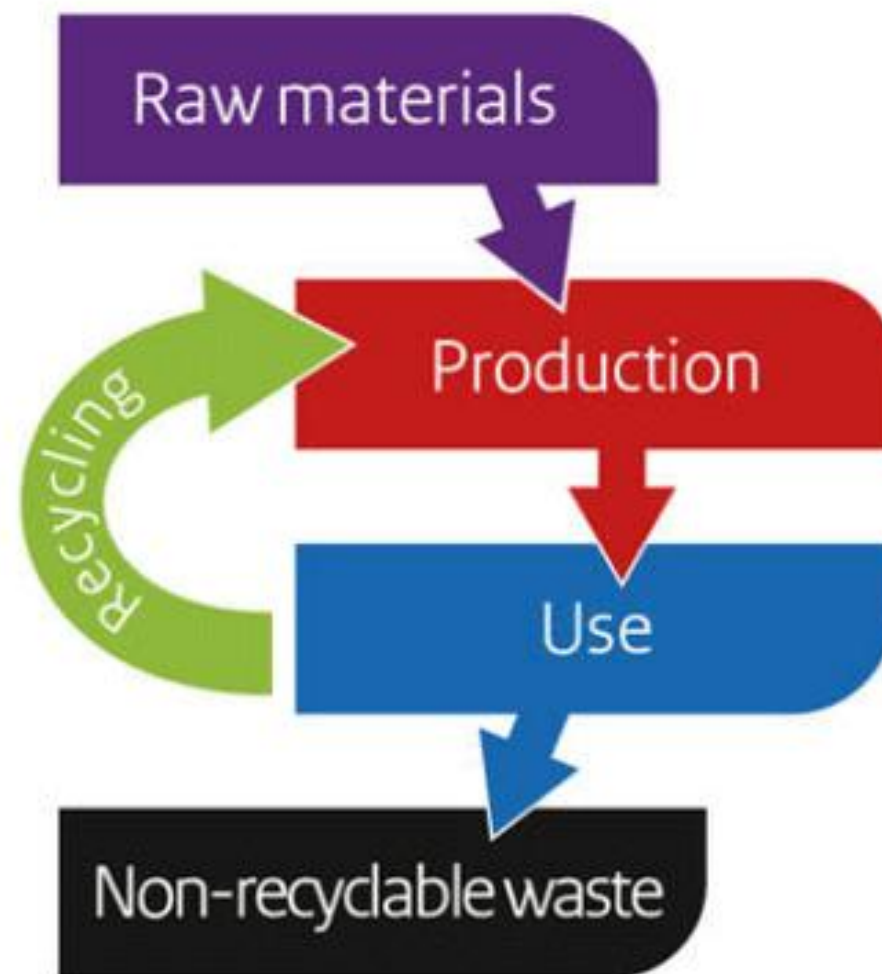


from a linear to a circular economy

Linear economy



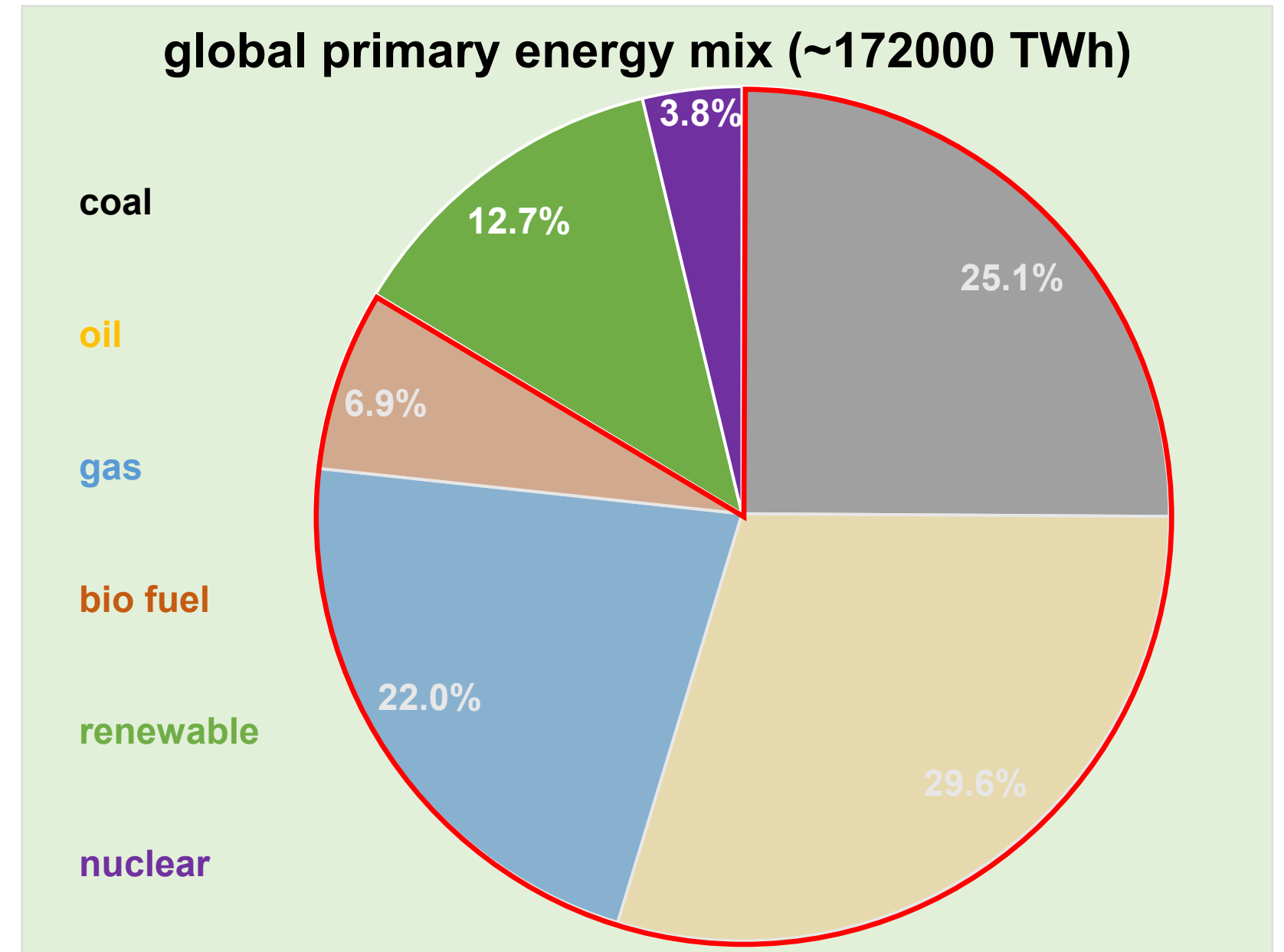
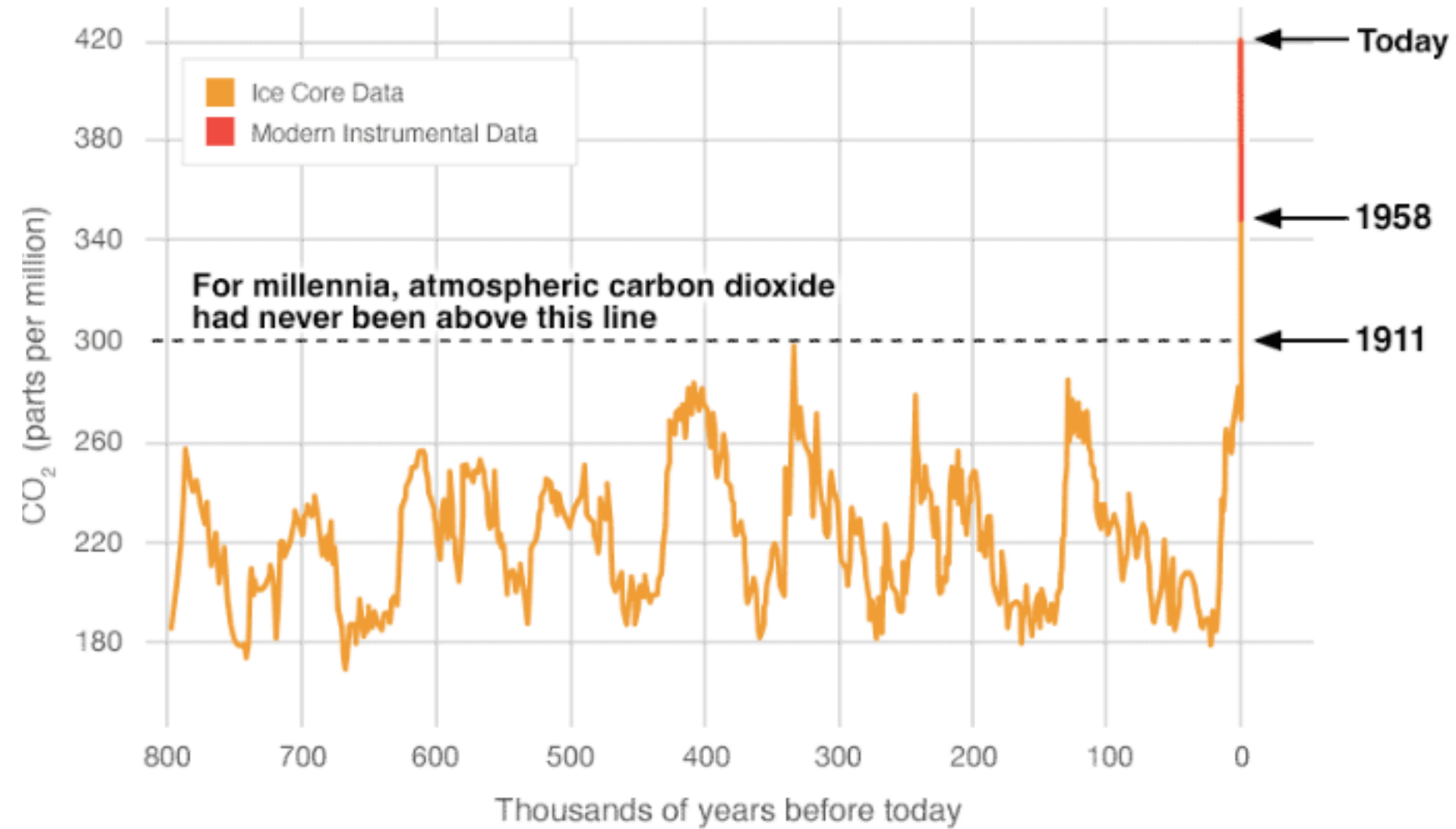
Reuse economy



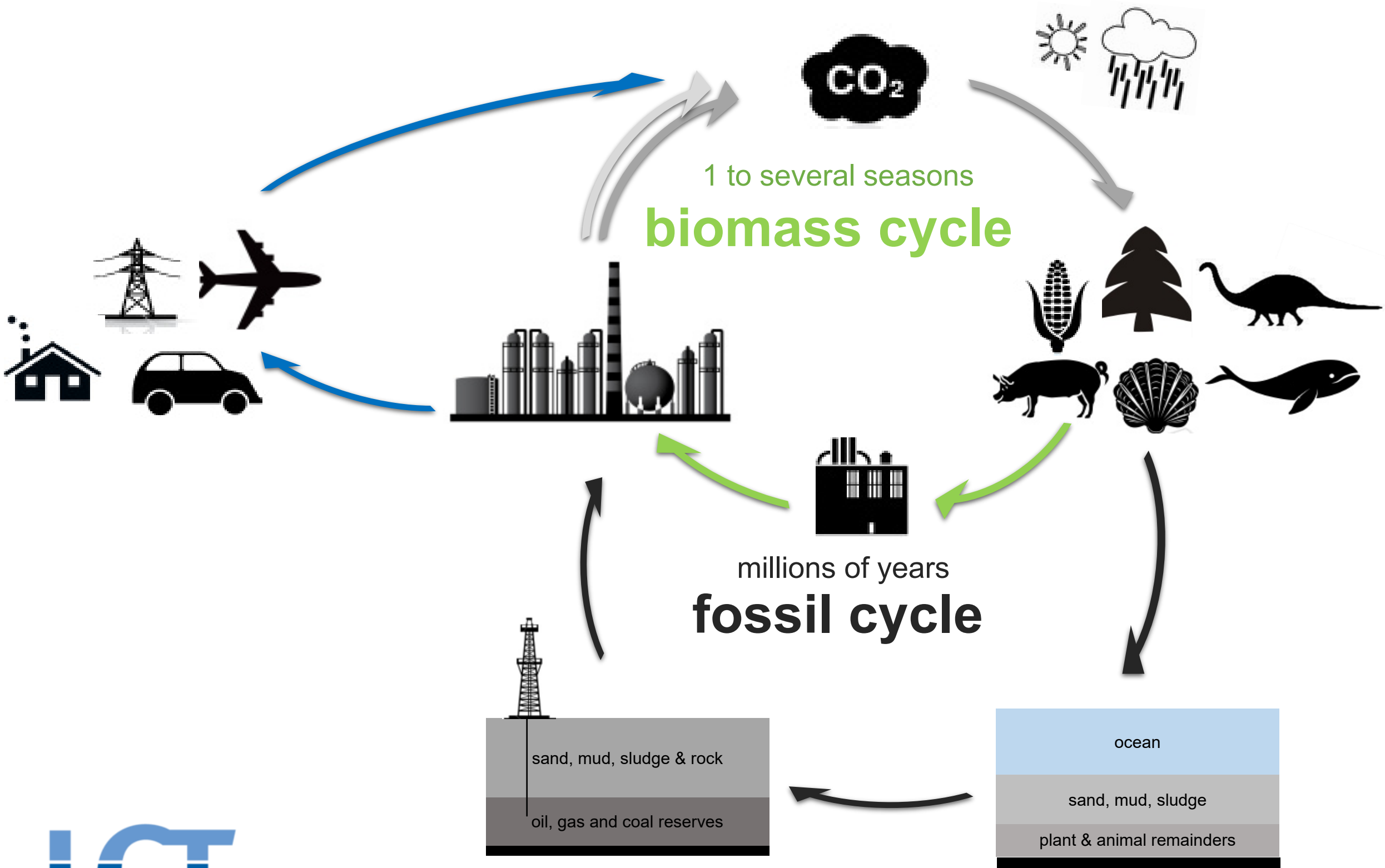
Circular economy



CO₂ challenge and energy transition



energy context



biomass cycle

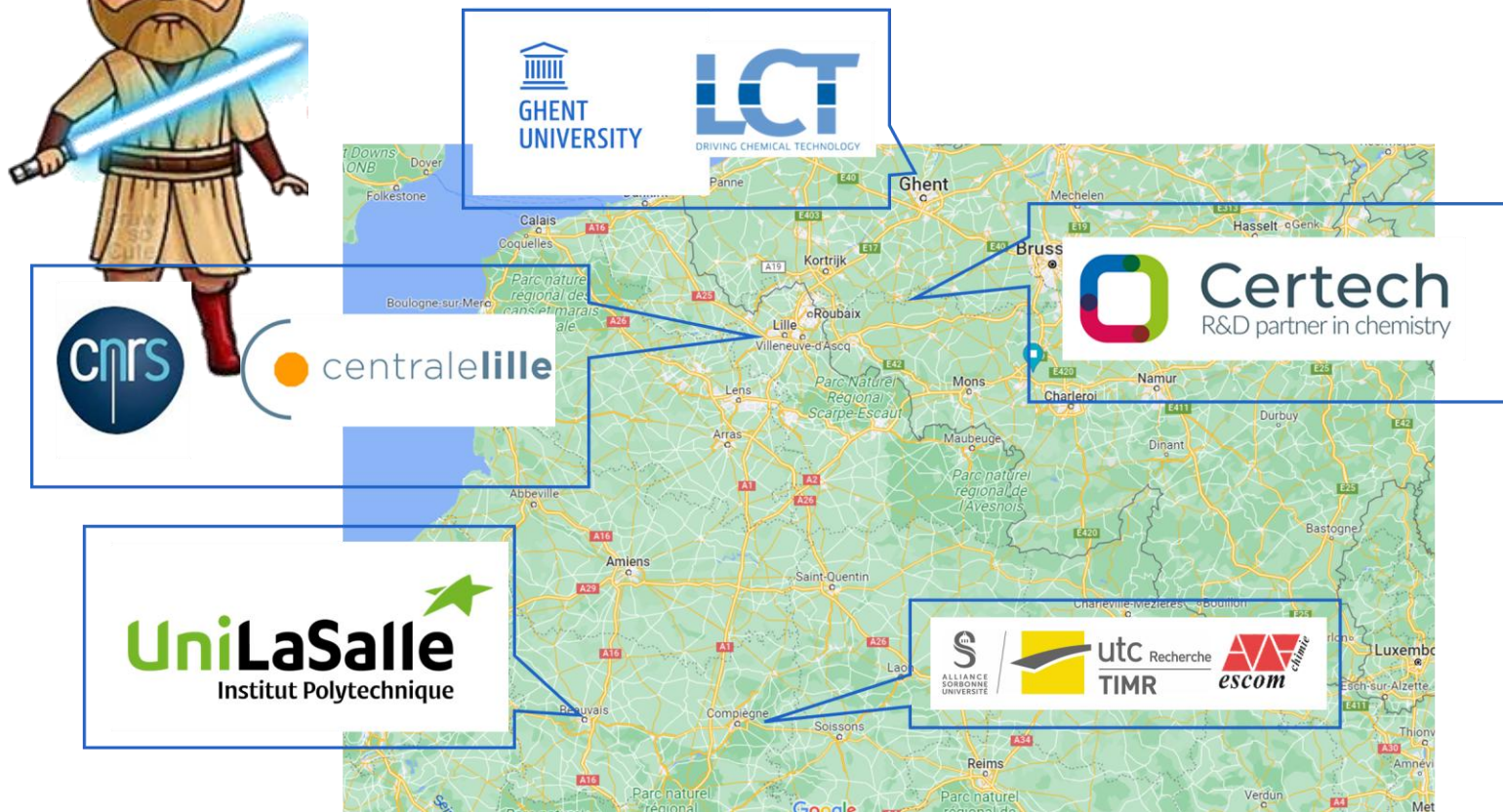
- thermochemical methods
 - gasification ($\text{CO} + \text{H}_2$)
 - pyrolysis (complex liquid oil)
 - hydrothermal liquefaction (complex liquid oil)
- biochemical methods
 - fermentation ($\text{CH}_4 + \text{CO}_2$)

outline

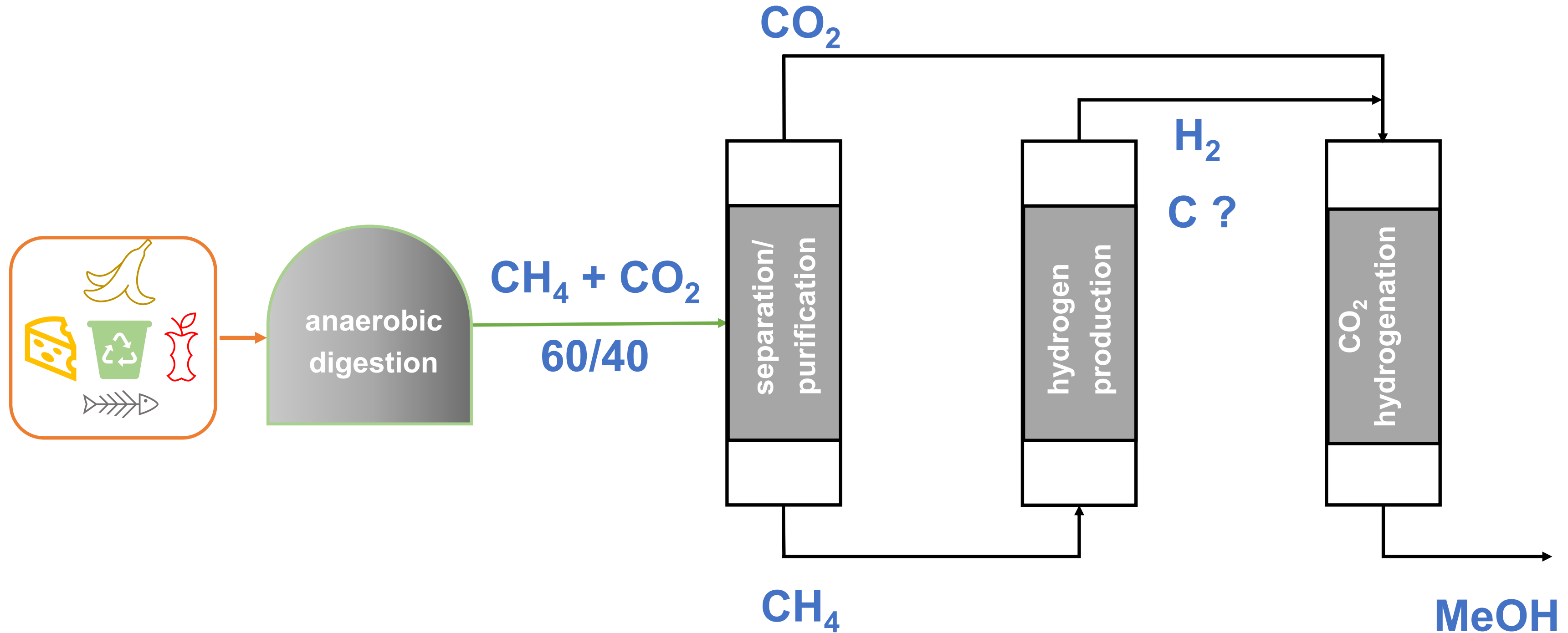
- introduction
- energy circularity
 - OBIWAN
 - STEROPE
- ElectroThermal Fluidized Bed reactor (ETFB)
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- conclusions & perspectives

OBIWAN: context

- biogas ($\text{CH}_4 + \text{CO}_2$) valorization
 - calorific
 - to chemicals/(sustainable aviation fuels)

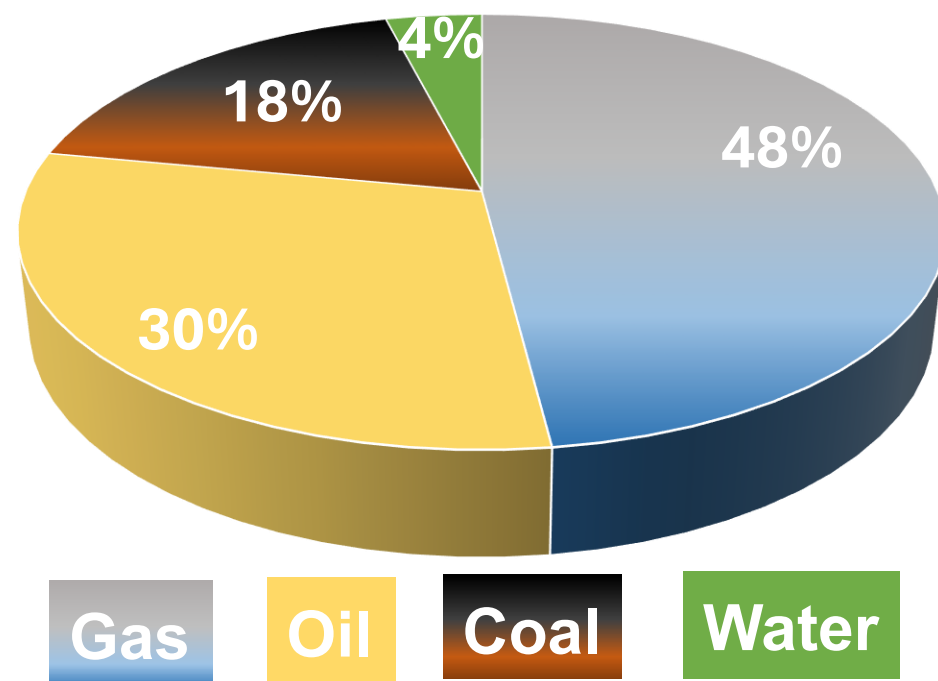


OBIWAN: process lay-out



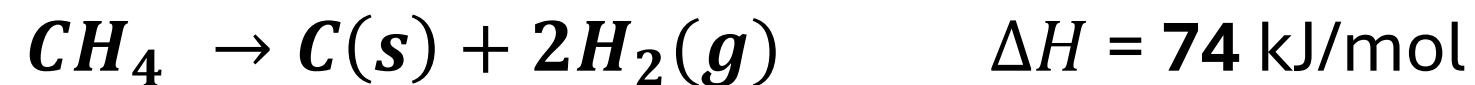
H₂ production technologies

H₂ production feedstocks



Technology	reaction	ΔH kJ/mol	cost (\$/kg)	GWP (kg CO ₂ eq)
Steam Methane Reforming SMR + CCS	$CH_4 + H_2O \leftrightarrow CO + 3H_2$	206	2.08	11.9
			2.27	3.7
Coal Gasification CG + CCS	$C + H_2O \leftrightarrow CO + H_2$	-130	1.34	22.9
			1.63	4.8
Electrolysis	$2H_2O \leftrightarrow 2H_2 + O_2$	285	>3	>0.7

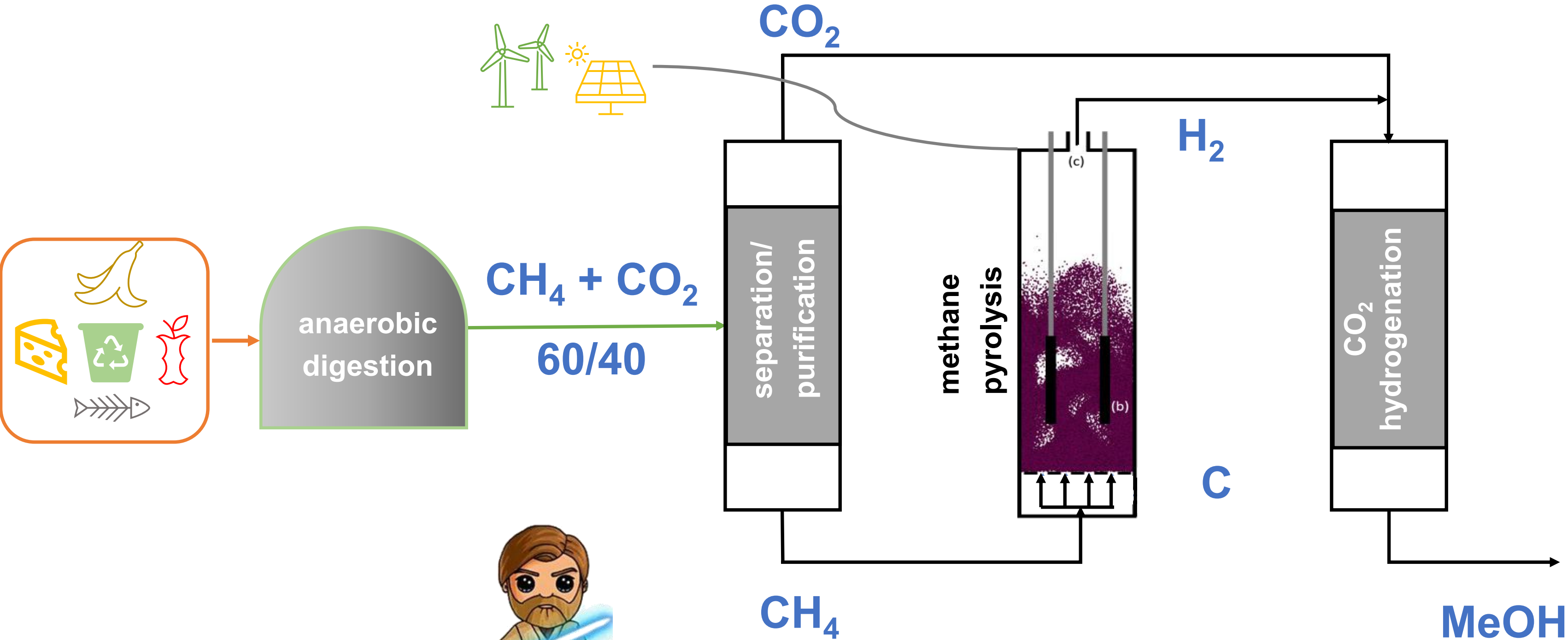
Catalytic Methane Decomposition:



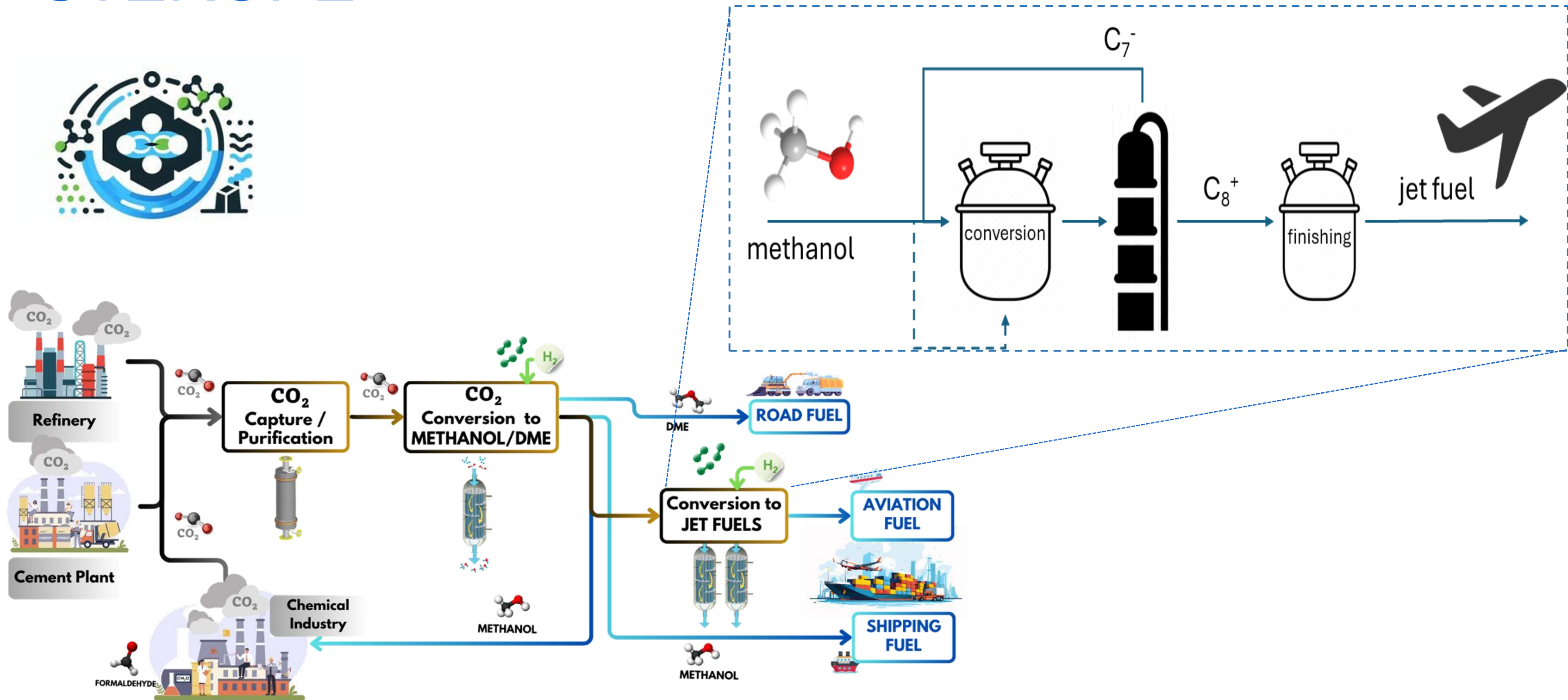
CDM on carbonaceous catalyst:

- ☐ less energy-intensive
- ☐ Less greenhouse gas emission
- ☐ Produces H₂ with high purity
- ☐ Cheap catalyst
- ☐ Sulfur-resistive catalyst

OBIWAN: process lay-out



STEROPE



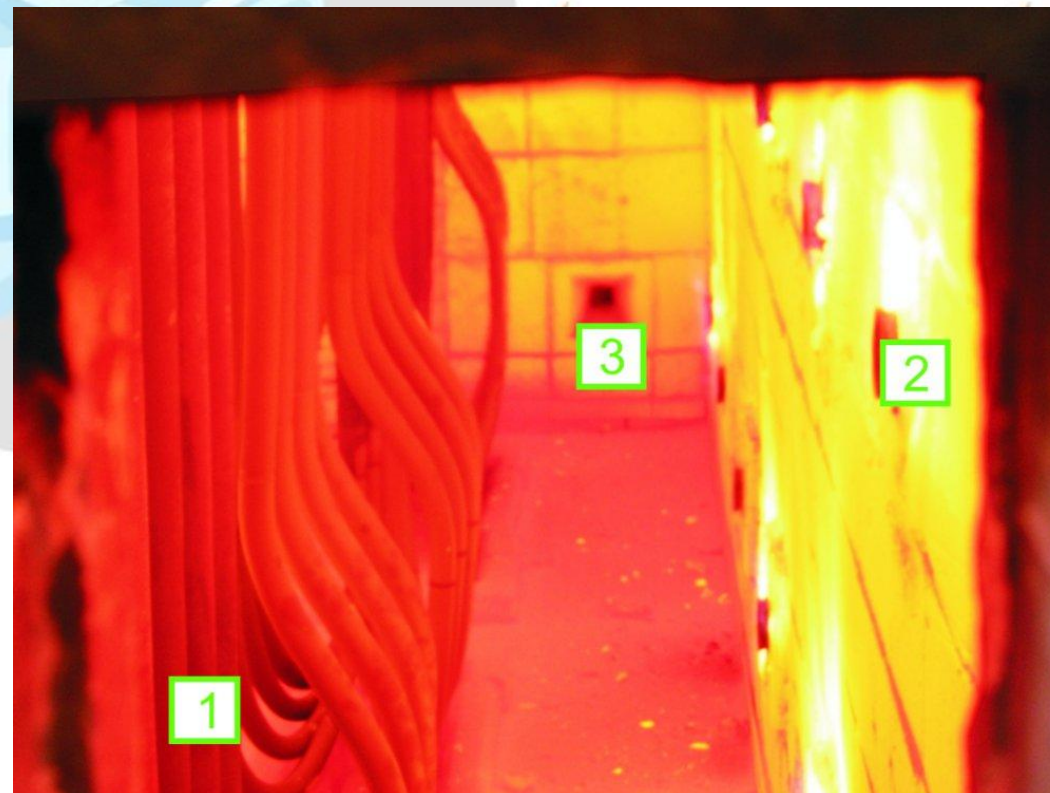
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heat requirements in chemical reactions

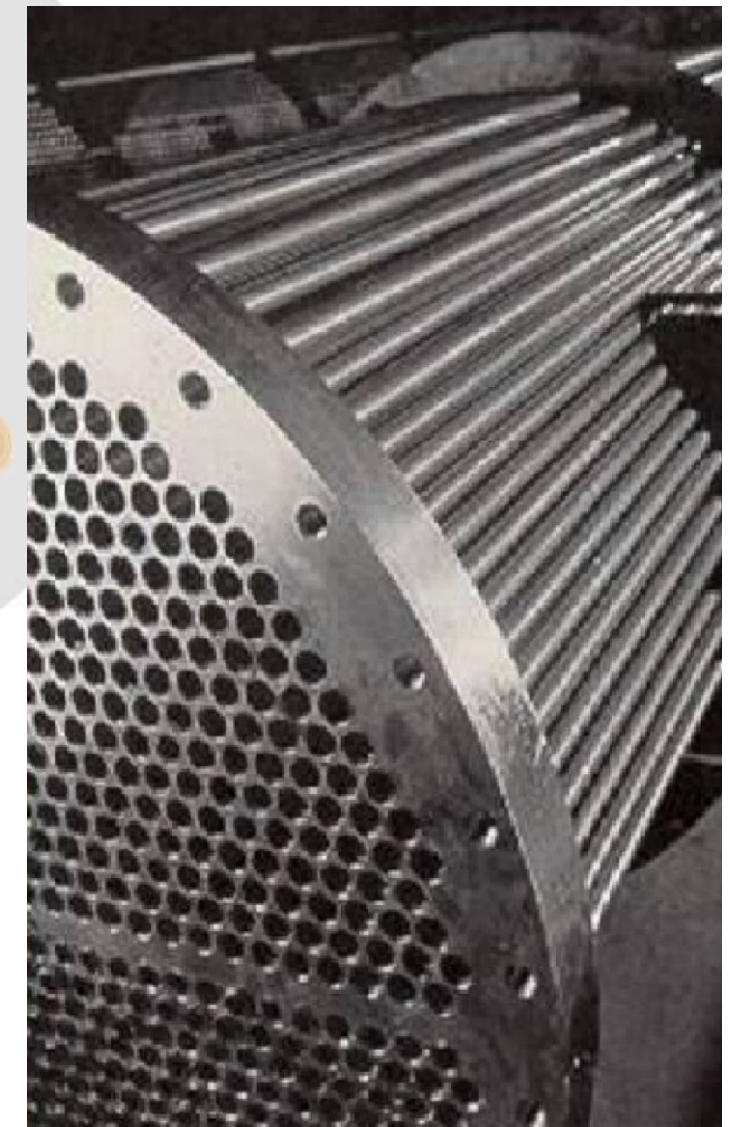
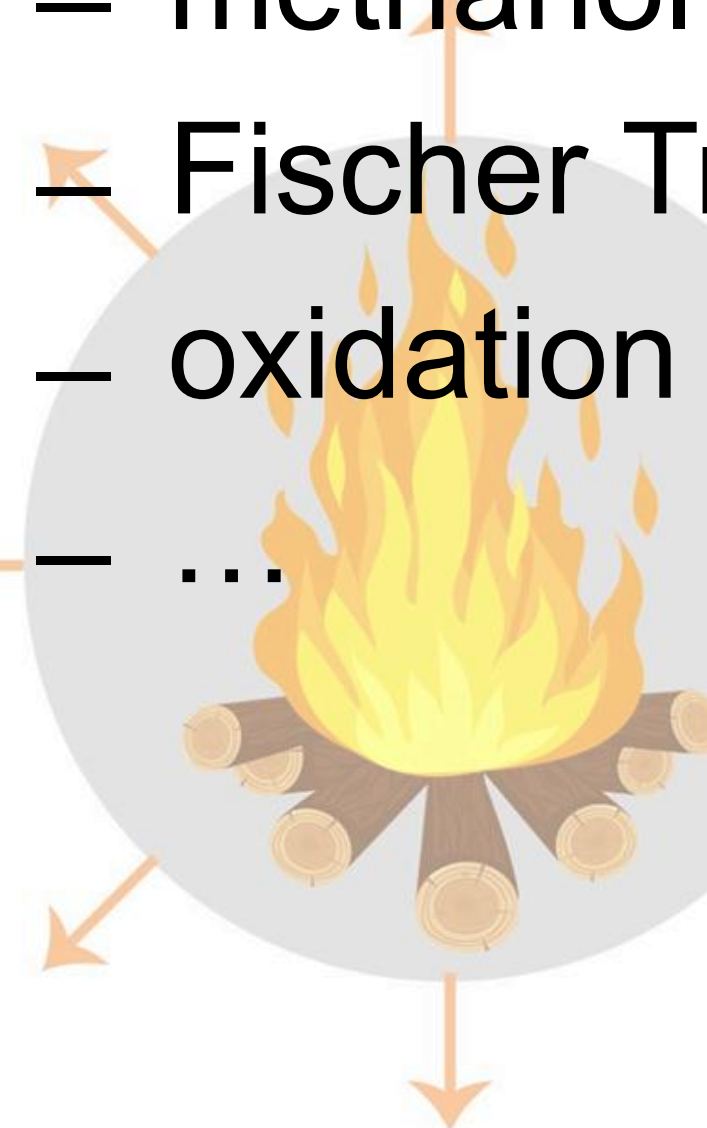
- endothermic reactions

- thermal cracking
- dehydrogenation
- reforming
- ...



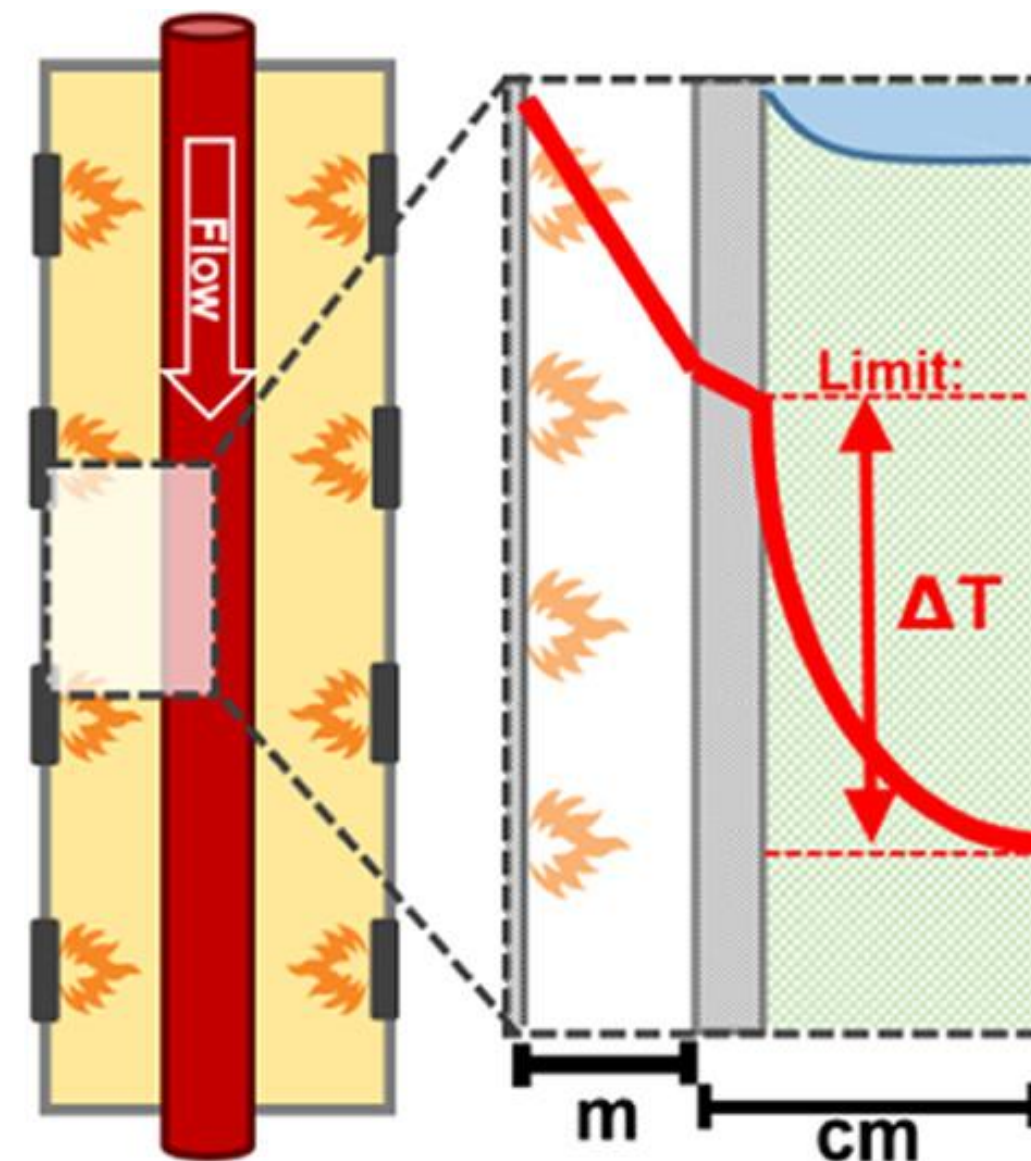
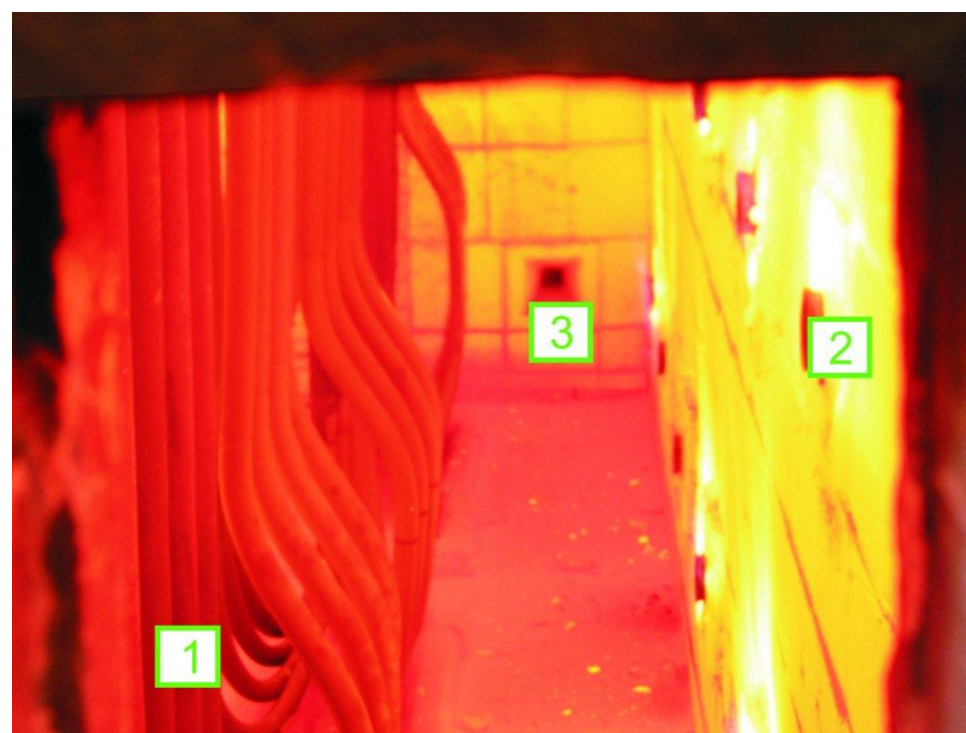
- exothermic reactions

- methanol synthesis
- Fischer Tropsch
- oxidation
- ...



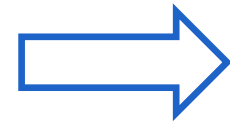
(strongly) endothermic reactions

- heat transport focused reactor design
- narrow tubes
- fired furnace
- pronounced temperature gradients



Wismann, et al. *Ind. Eng. Chem. Res.* 58 (2019) 23380

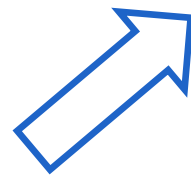
how can we enhance heat transfer?



heat containment

electrification

how can we do even better?



microwave



induction

**heating from
the inside**

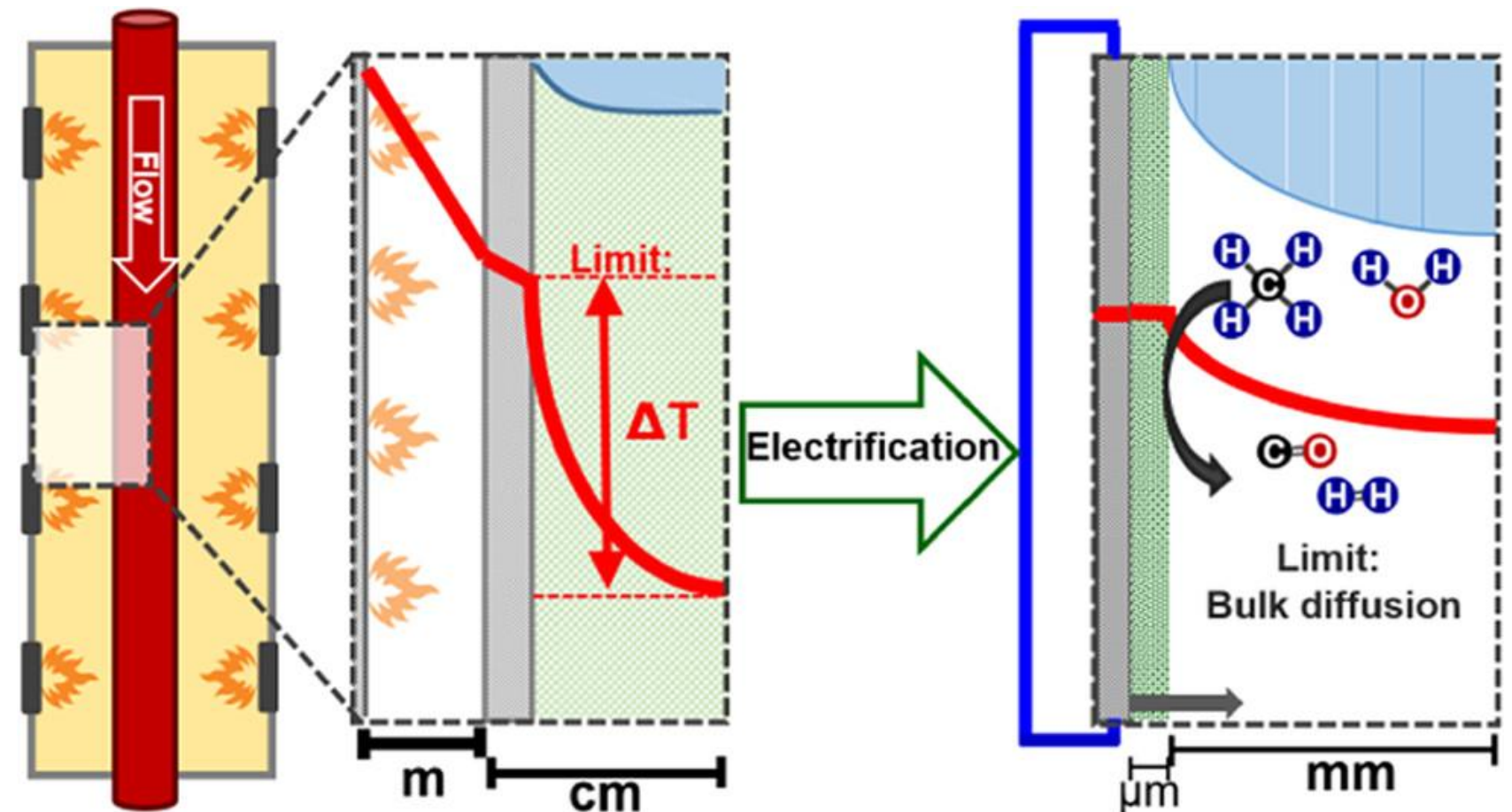


reactor electrification

electrical heating -> overcoming limitations of combustion in furnaces

advantageous in terms of:

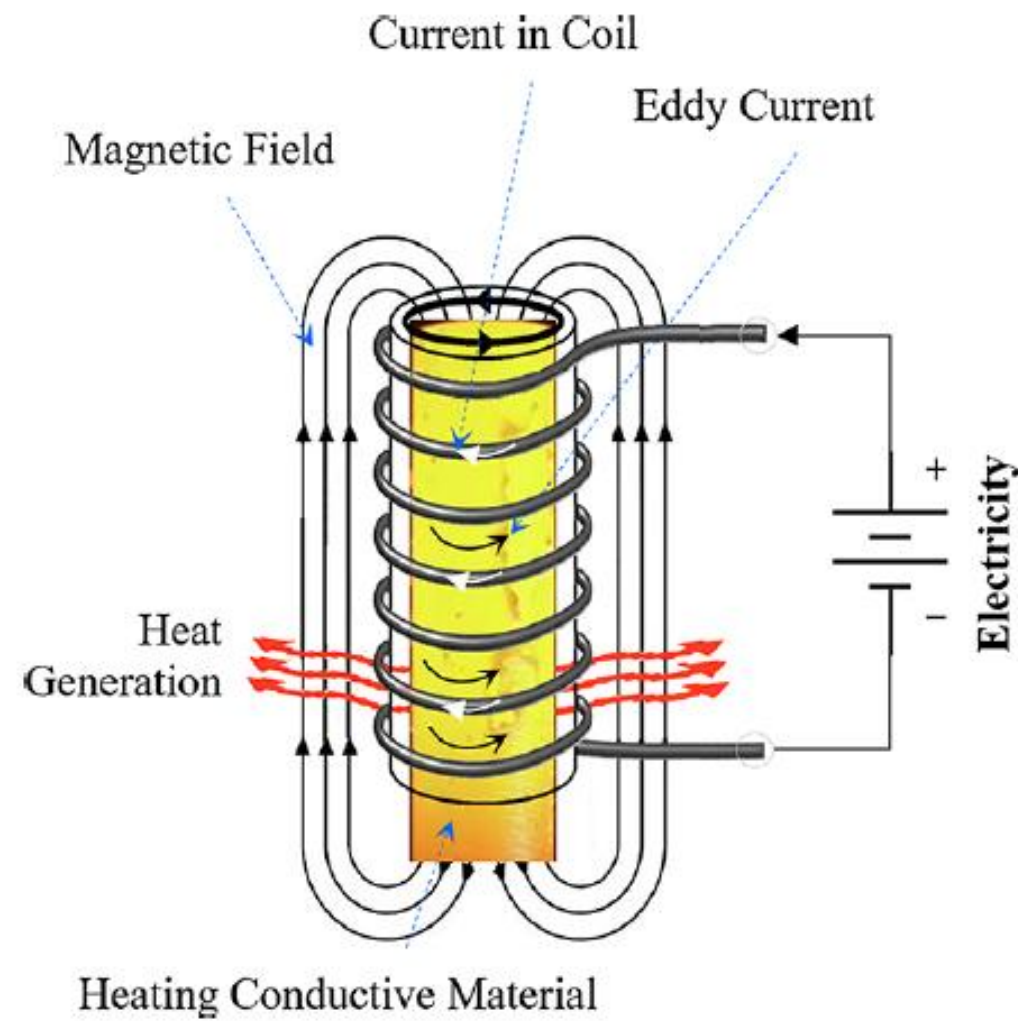
- energy efficiency
- process control
- safety and maintenance
- rapid heating
- ...



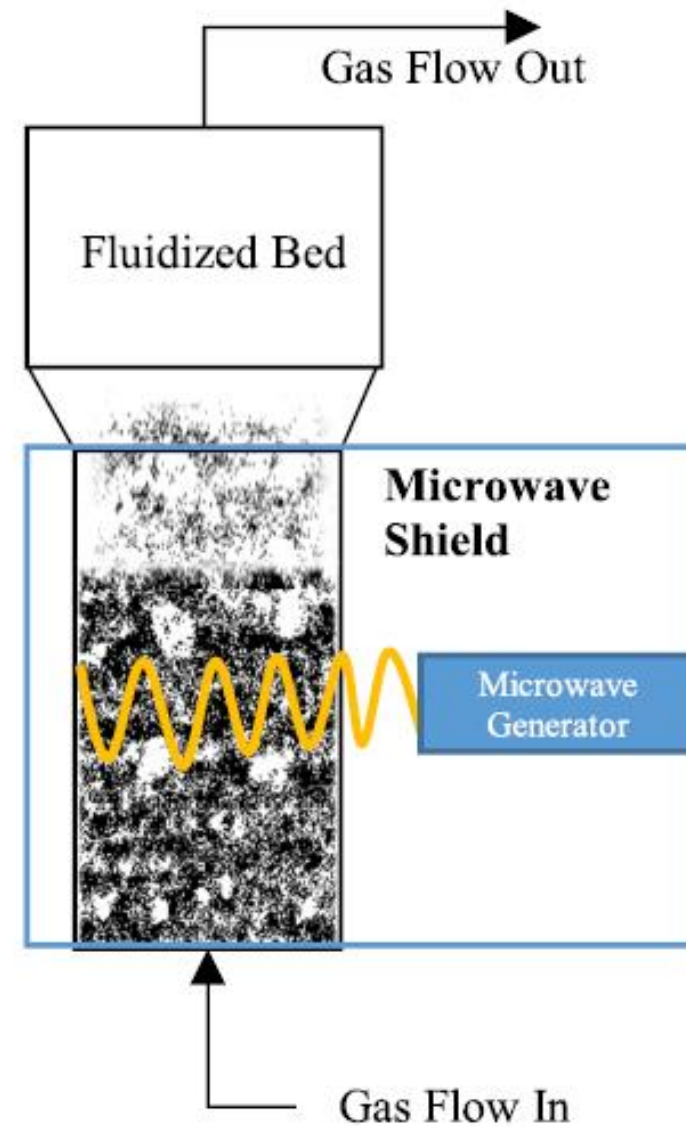
Wismann, et al. *Ind. Eng. Chem. Res.* 58 (2019) 23380

electrical heating

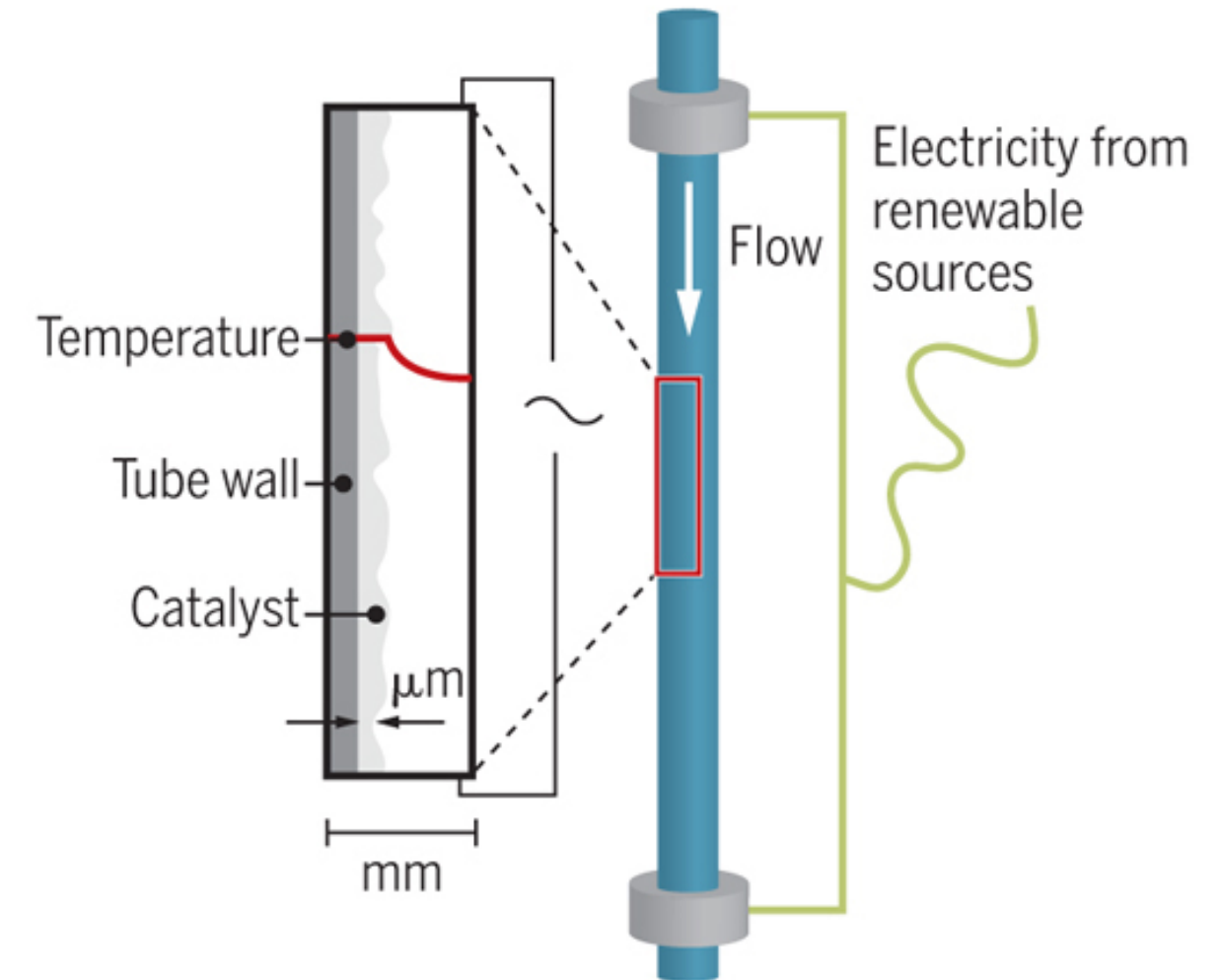
induction



microwave



Joule

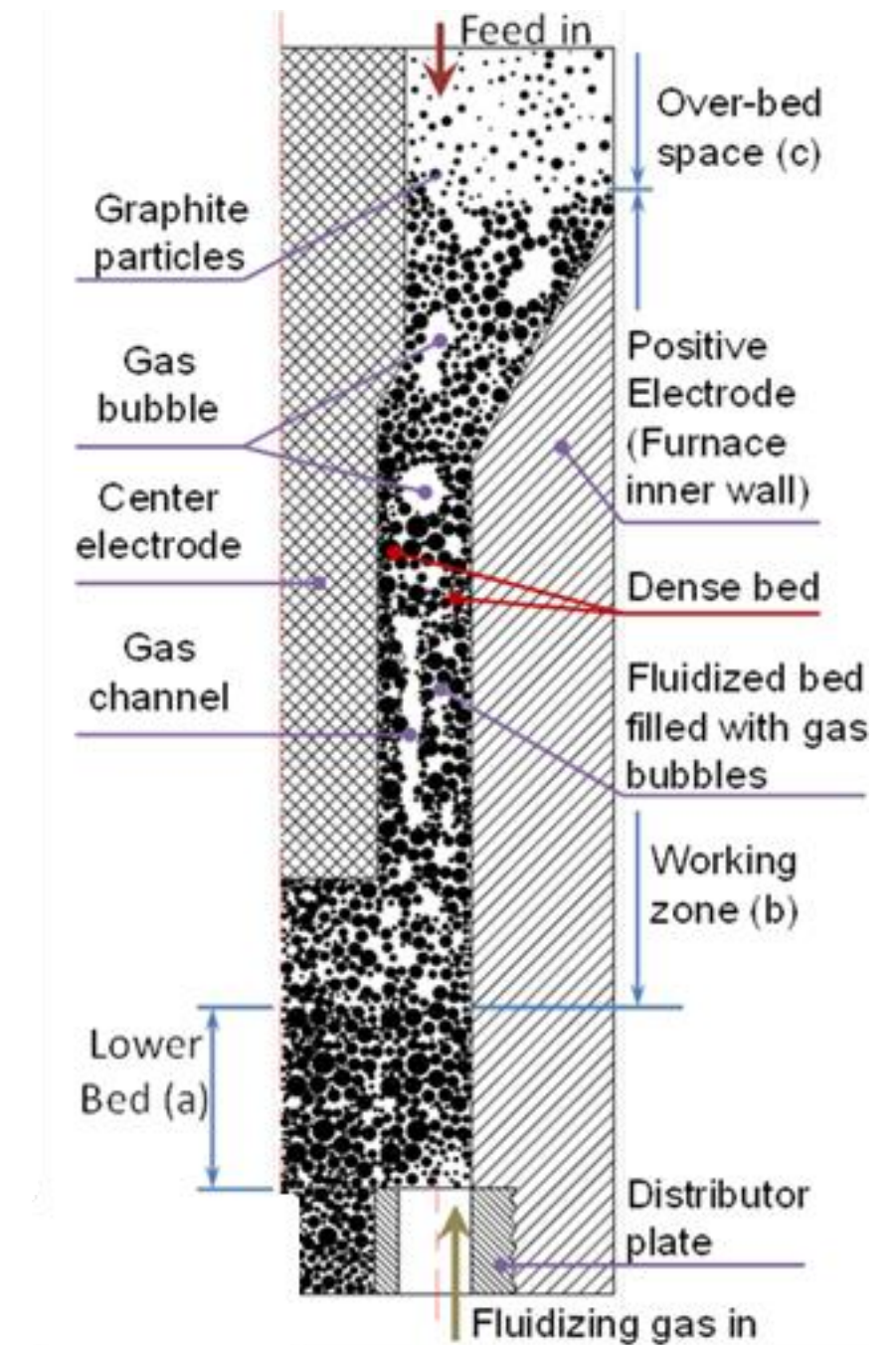


sonication plasma

Imtiaz, et al. *Ind. Eng. Chem. Res.* 63 (2024) 4205

ElectroThermal Fluidized Bed reactor (ETFB)

- combination:
 - fluidization
 - Joule heating
- compared to conventional fluidized beds
 - better control over bed temperature
 - highly energy efficient
 - rapid and uniform heating

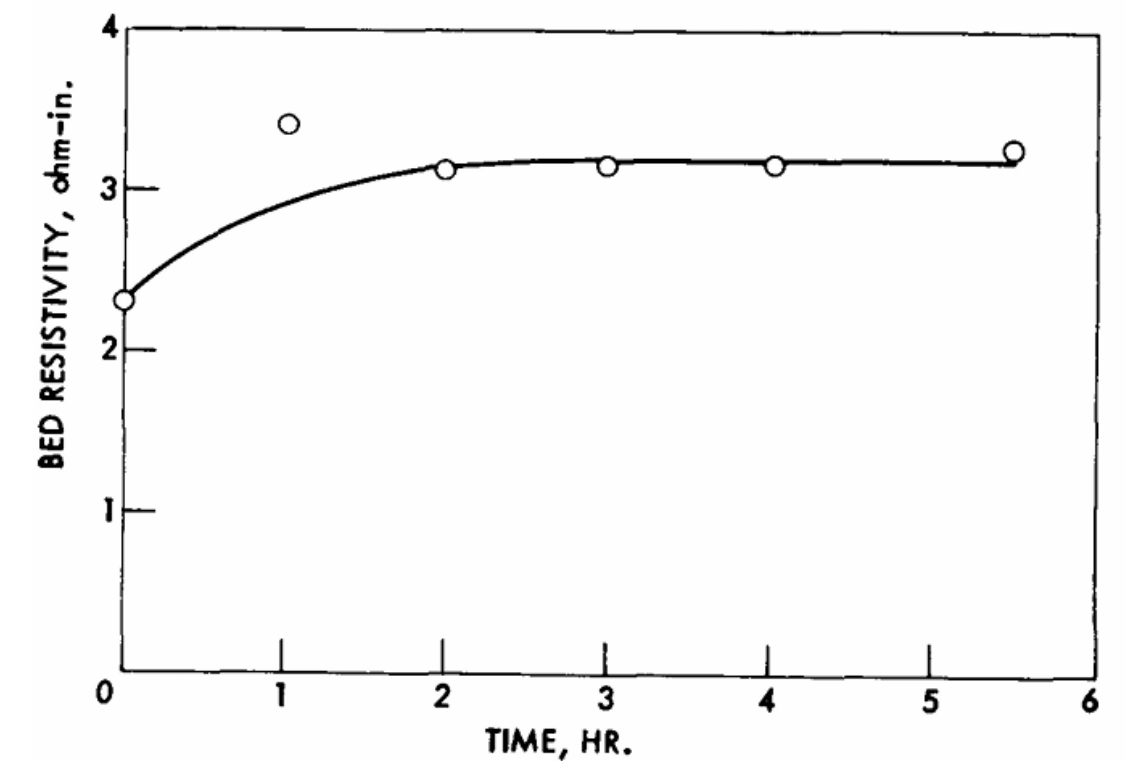
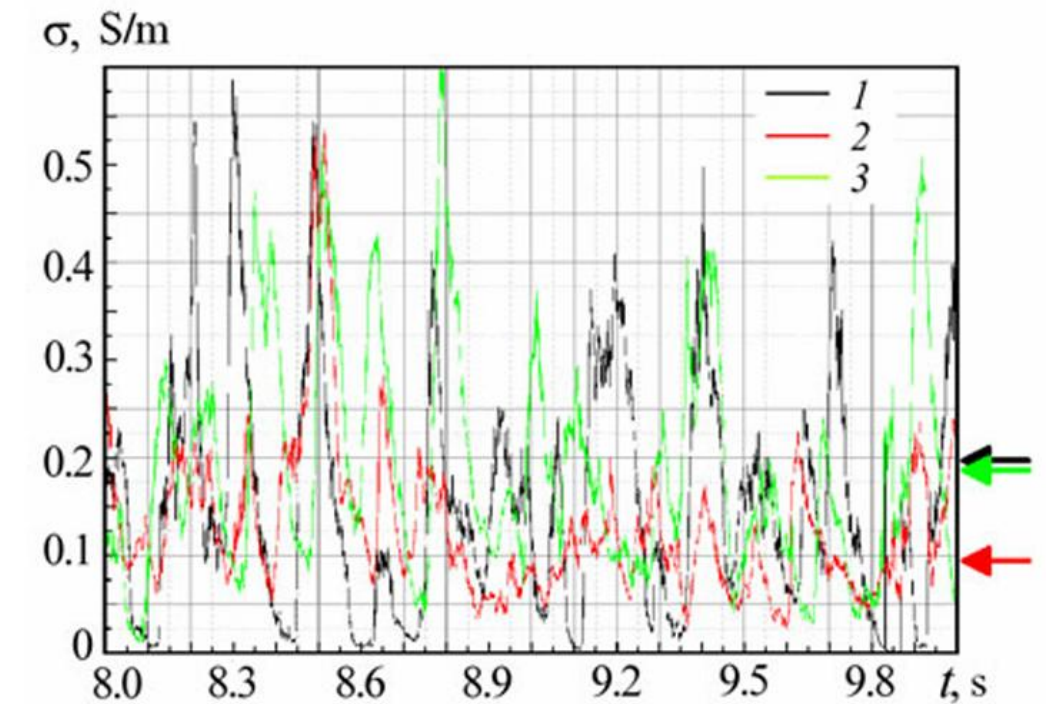
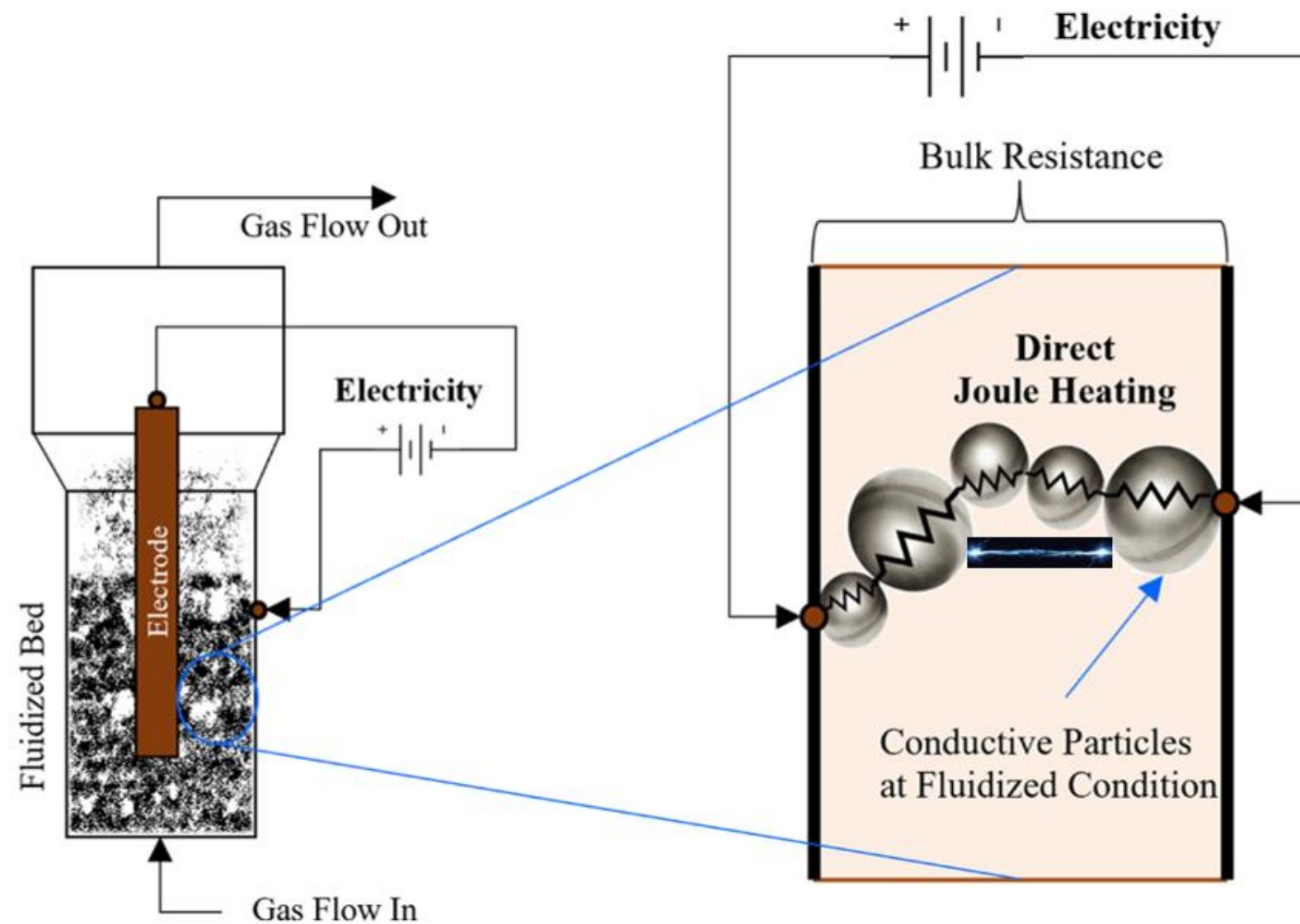


Fedorov *J. Fluids Eng.* 138 (2016) 044502

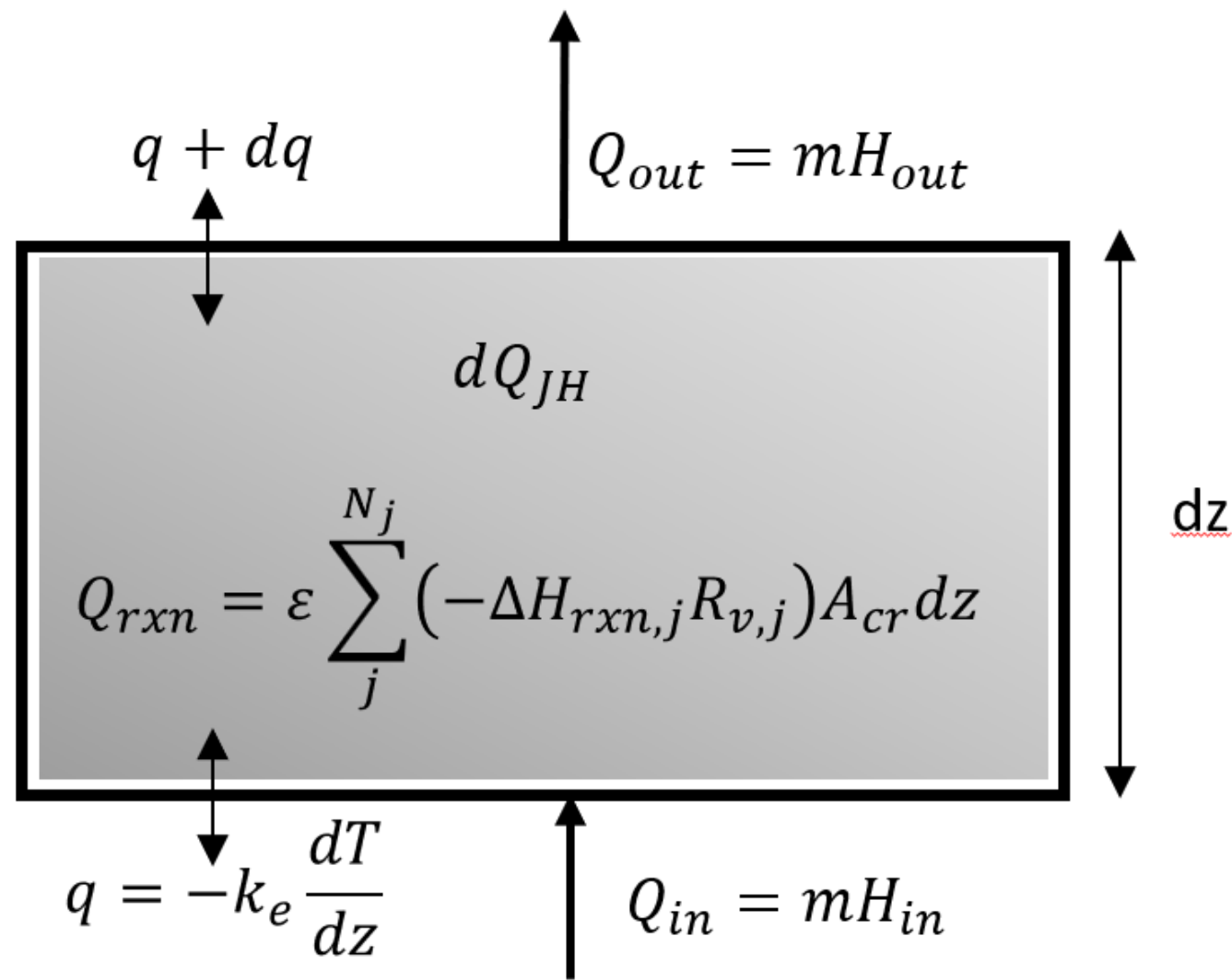
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Joule heating in a fluidized bed



ETFB reactor heat balance



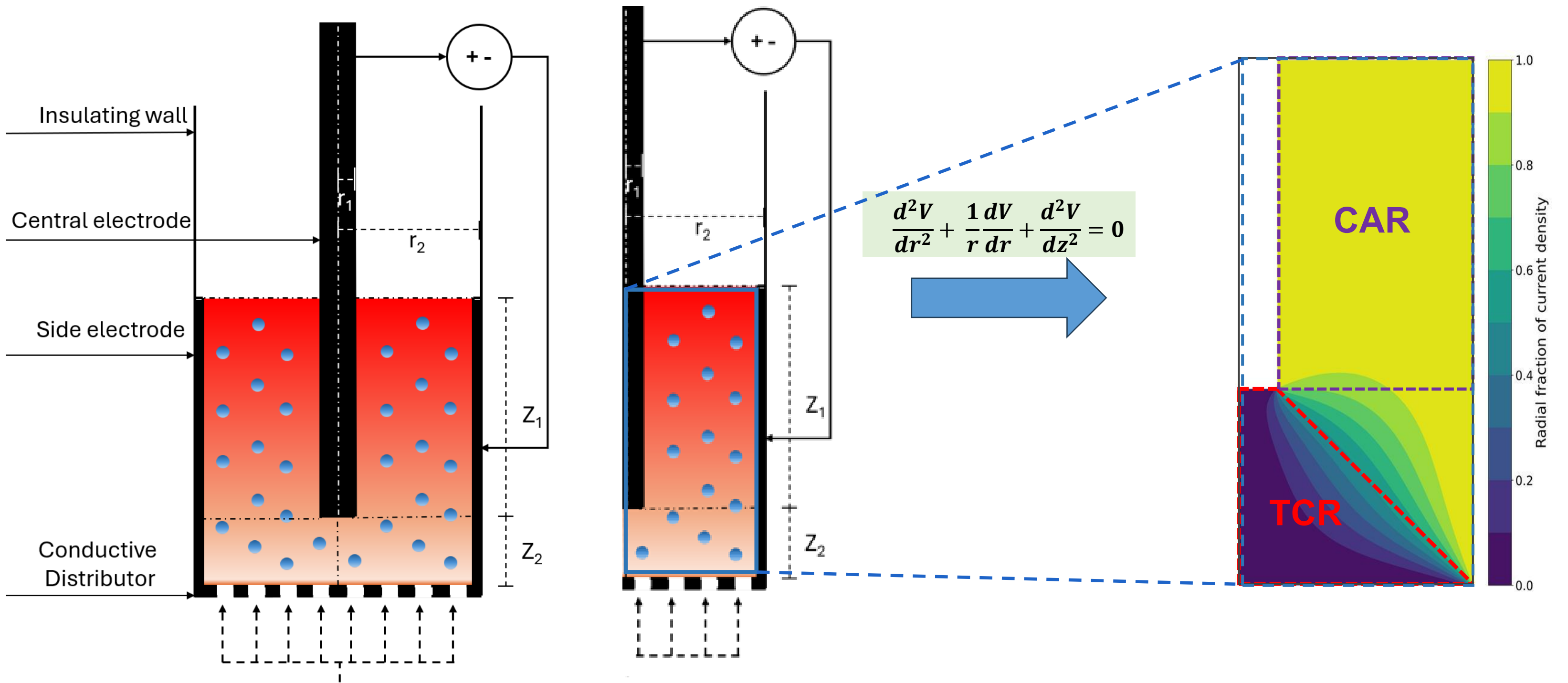
$$u\rho_g C p_g \frac{dT}{dz} - k_e \frac{d^2T}{dz^2} - \varepsilon \sum_j^{N_j} (-\Delta H_{rxn} R_{v,j}) - \frac{dQ_{JH}}{dz A c_{reactor}} = 0$$

convection conduction heat of reaction heat generation
 $\rightarrow$ Joule heating term

assumptions

- bubbling fluidization regime
- low- and high-density phases are at the same temperature
- no radial profiles
- constant effective conductivity at average temperature and composition
- adiabatic operation
- steady state operation

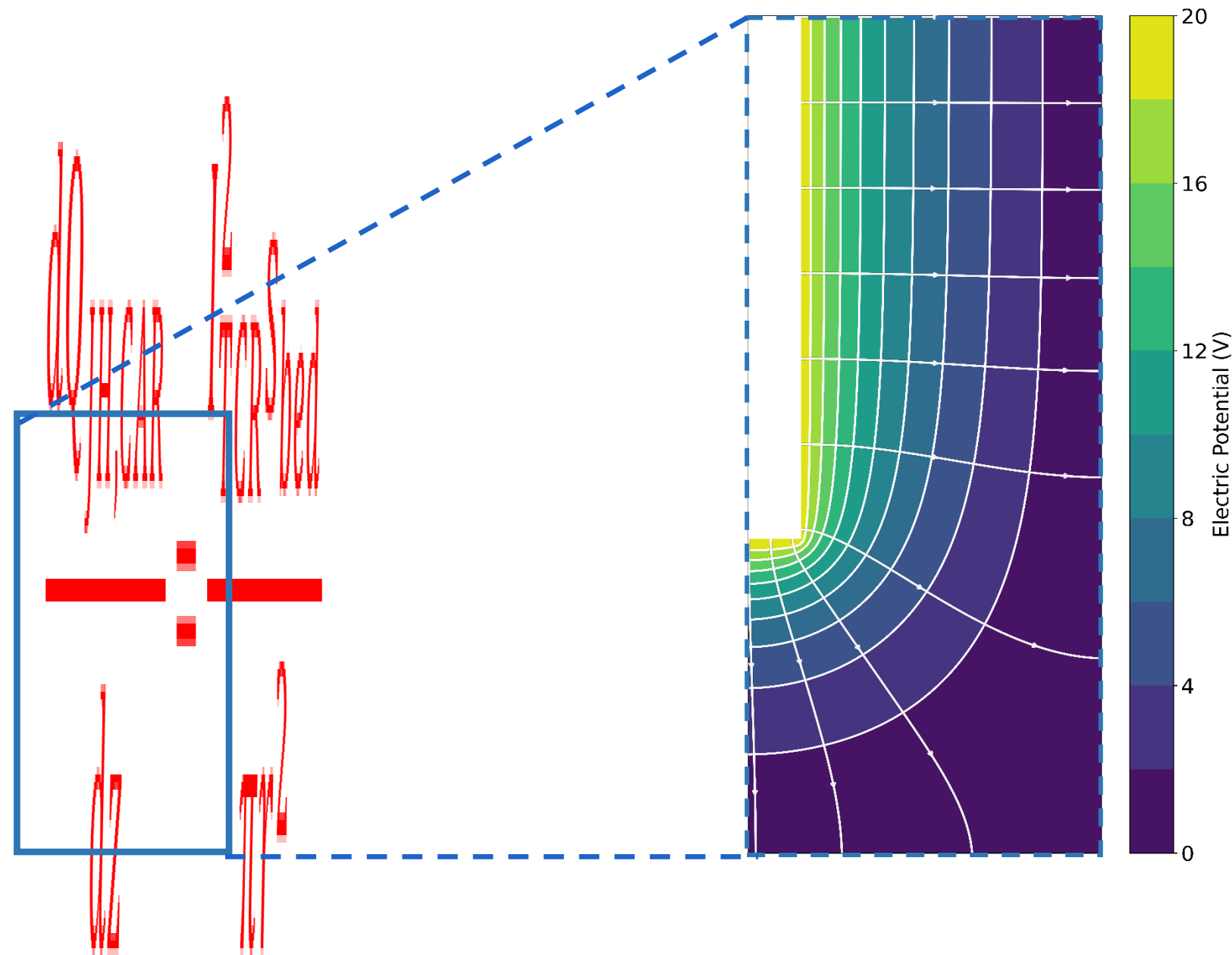
ETFB electrical field



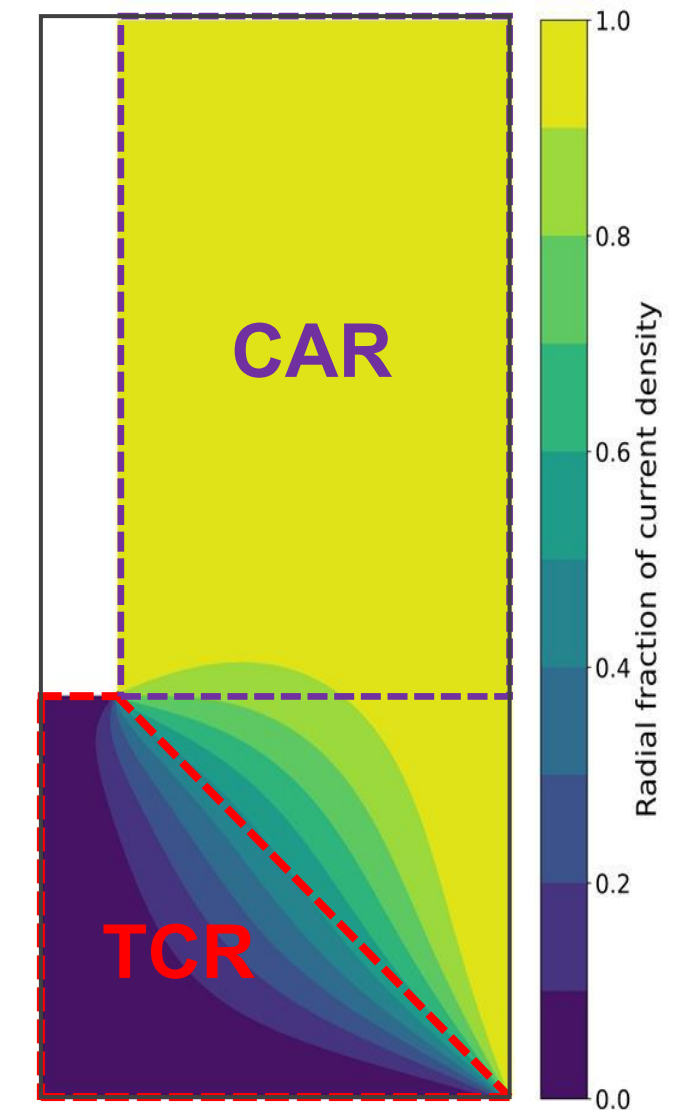
truncated cone resistor

ETFB electrical field modeling

Laplacian Field (LF)



Current Partitioning (CP)



$$\frac{dQ_{JH}}{dz} = \int_0^R -\frac{2\pi}{s_{bed}} \left(\left(\frac{d\Delta V}{dr} \right)^2 + \left(\frac{d\Delta V}{dz} \right)^2 \right) r dr$$

$$\frac{dQ_{JH,CAR}}{dz} = \frac{V^2 2\pi}{s_{bed} \ln\left(\frac{r_2}{r_1}\right)}$$

$$\frac{dQ_{JH,CAR}}{dz} = \frac{I_{TCR}^2 s_{bed}}{\pi r^2}$$

CH₄ pyrolysis in ETFB reactor

power density profile

$$\text{CH}_4 = 0.72 \text{ kg hr}^{-1}$$

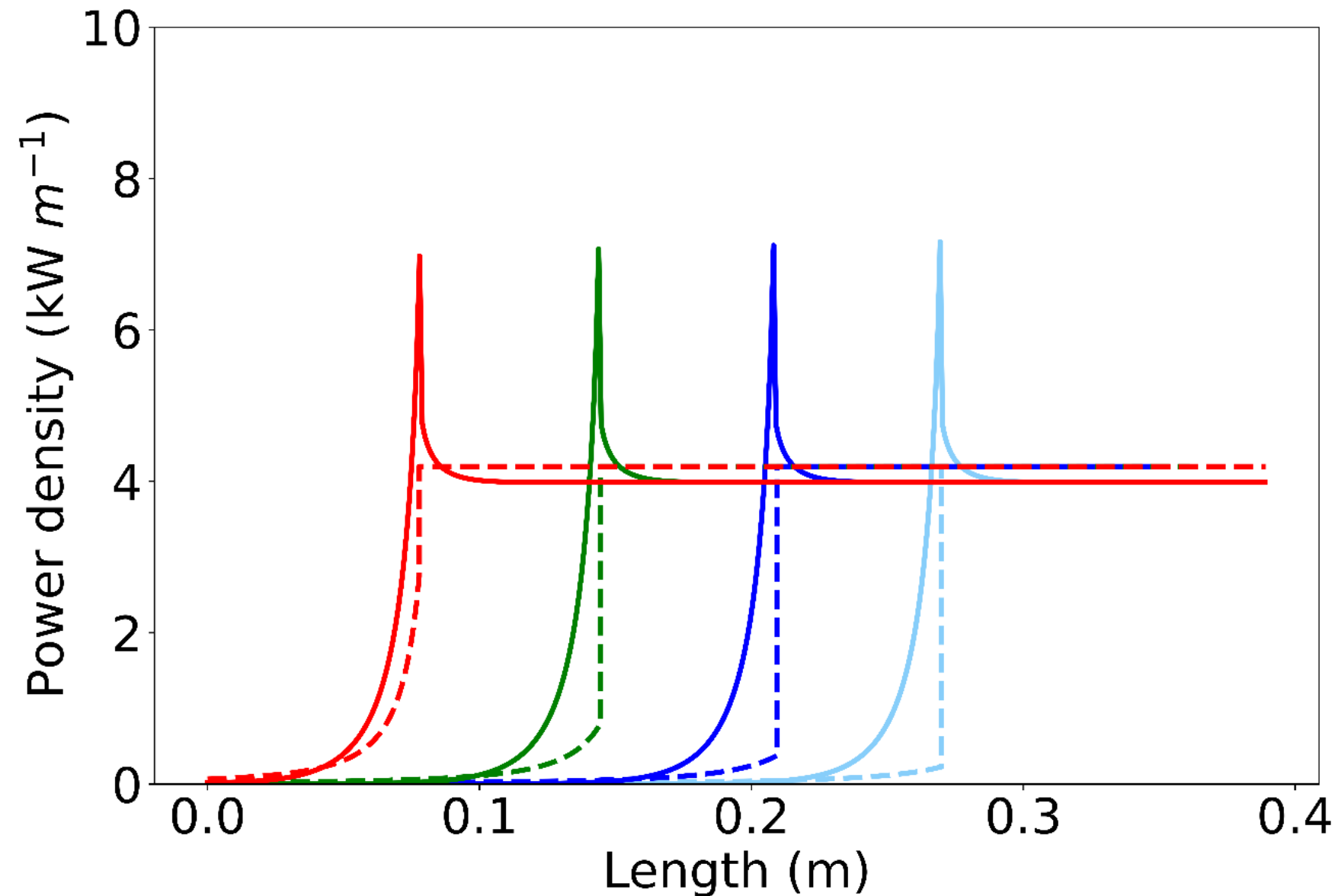
$$T_{\text{in}} = 600^\circ\text{C}$$

$$P = 1 \text{ atm}$$

$$ST = 1 \text{ kg h m}^{-3}$$

$$\sigma = 50 \Omega \cdot \text{cm}$$

$$\Delta V = 20 \text{ V}$$



electrode submersion

- 68 mm
- 140 mm
- 217 mm
- 312 mm

model

- Current Partition
- Laplacian Field

CH₄ pyrolysis in ETFB reactor

temperature profile

$$\text{CH}_4 = 0.72 \text{ kg hr}^{-1}$$

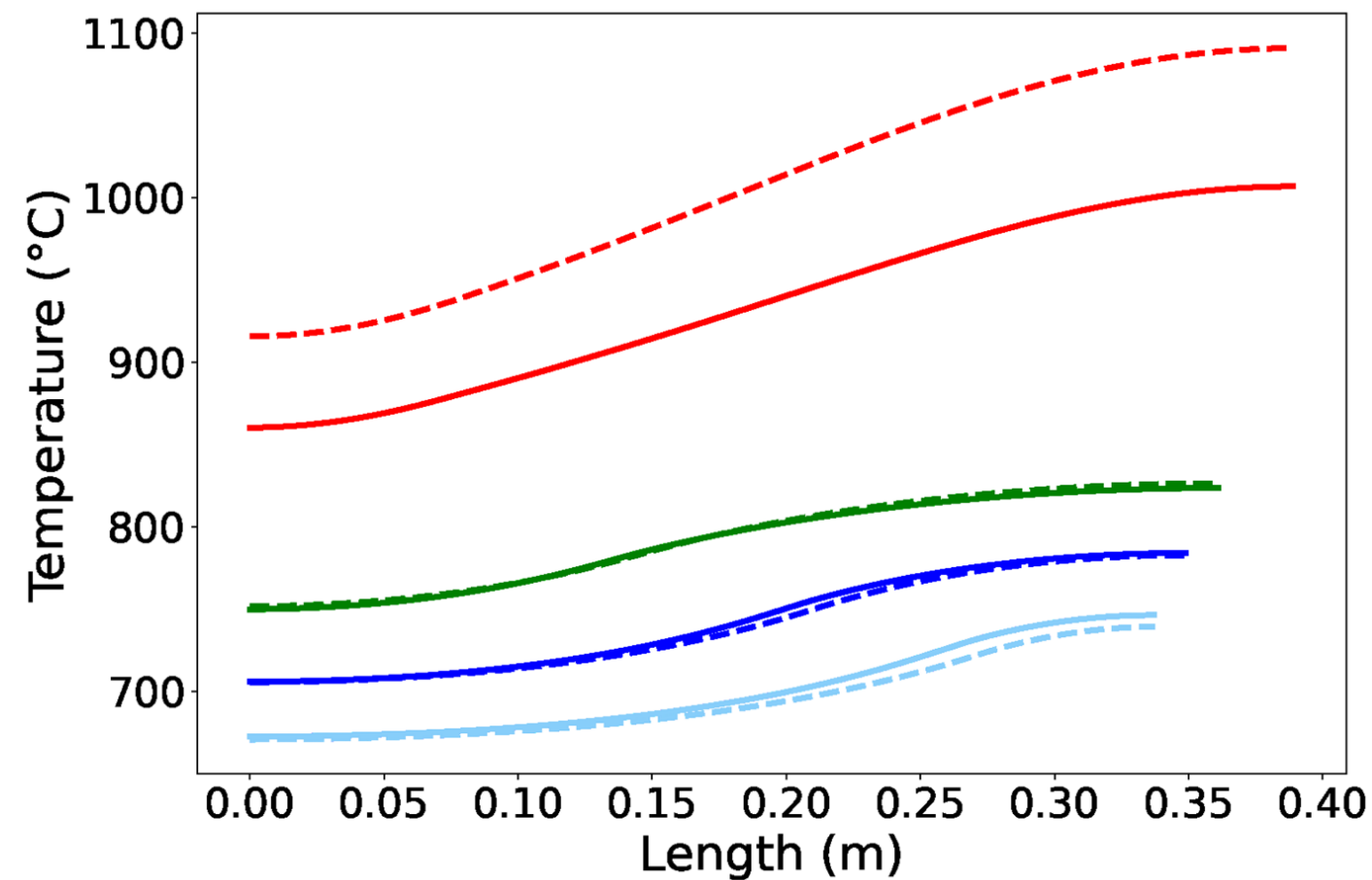
$$T_{\text{in}} = 600^\circ\text{C}$$

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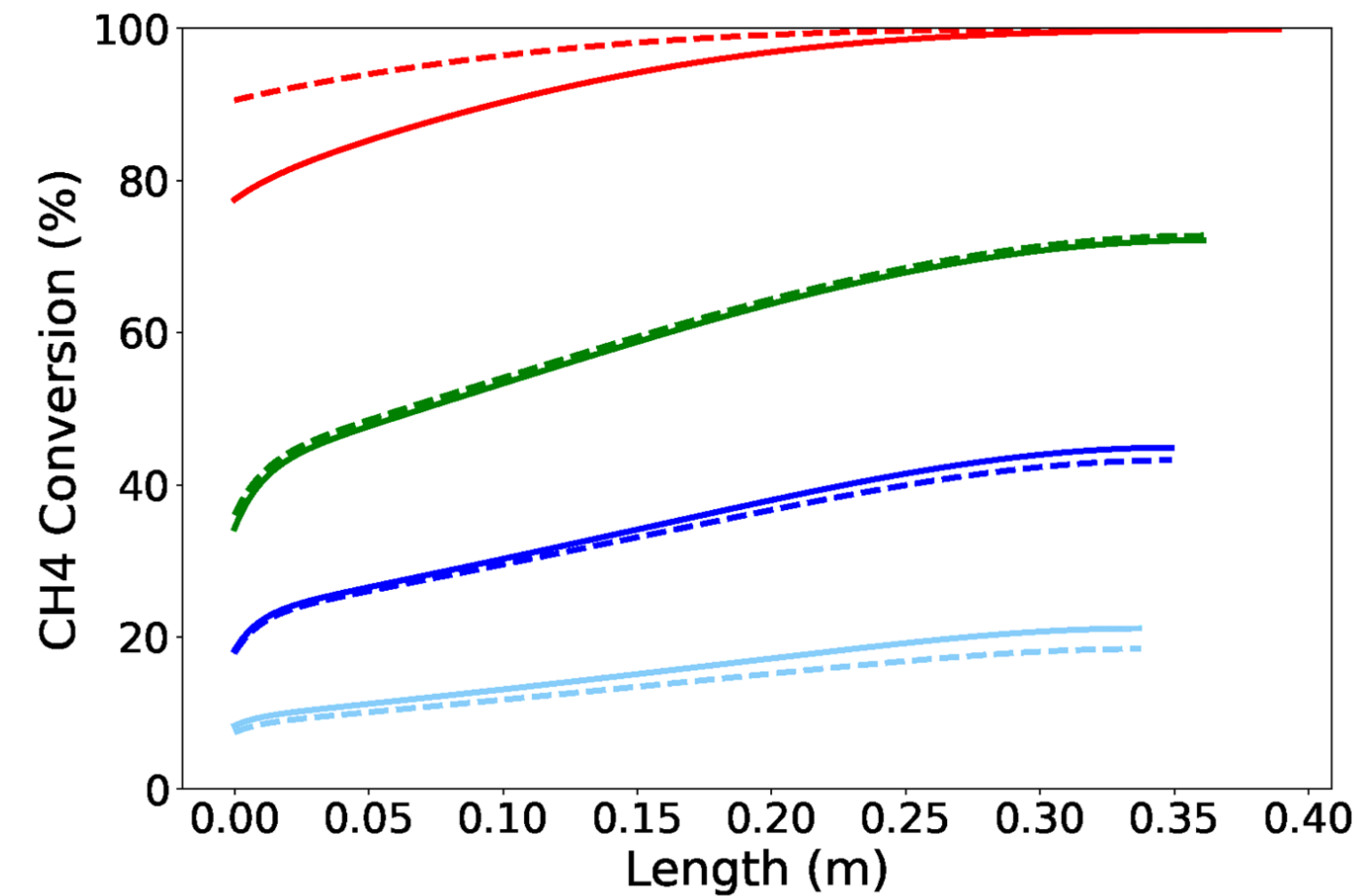
$$\Delta V = 20\text{V}$$



electrode submersion

- 68 mm
- 140 mm
- 217 mm
- 312 mm

CH₄ conversion profile



model

- Current Partition
- Laplacian Field

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conclusions

From Waste Treatment to Fuel Production: Ensuring Energy Circularity

- waste
 - biomass
 - forestry & agricultural residues
 - excess sludge from waste water treatment
- treatment via biogas production
 - CO₂ hydrogenation
 - H₂ obtained from CH₄ pyrolysis
 - reactor electrification:
 - heating from inside: “electricity is in the catalyst”
 - ElectroThermal Fluidized Bed (ETFB) reactor
- fuel production (for endothermic reactions):
 - Sustainable Aviation Fuels (SAF) ...

Interreg



Cofinancé par
l'Union Européenne
Medegefinancierd door
de Europese Unie

France - Wallonie - Vlaanderen



OBIWAN

Sterope

perspectives and challenges

- other waste
 - plastics
 - pyrolysis
 - hydrotreatment
 - treatment adapted to type of waste
- global treatment scenarios
 - distributed production
 - centralized processing
 - where to transition between both?
- challenges
 - few large-scale vs many small-scale applications
 - (renewable) electricity availability
 - impact on chemistry
 - ...

acknowledgments



The e-CODUCT and STEROPE projects are funded under Horizon Europe Grant Agreements n°101058100 and 101235659



Interreg



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l'Union Européenne
Medegefinancierd door
de Europese Unie

France – Wallonie – Vlaanderen



OBIWAN

The OBIWAN is funded under Grant Agreement n°0100186

acknowledgements (2)

(former) post docs

Ana Bjelic

Jeroen Lauwaert

Jeroen Poissonnier

Pedro Mendes

Soroush Zareghorbaei

Zahra Mohammadbagheri

(former) PhD students

Alejandro Romero Limones

Alexandra Bouriakova

Anoop Chakkingal

Bert Biesemans

Beruk Alemu Bekele

Bram Van Wettere

Carlos Alvarado Camacho



César Pernalete

Kevin De Ras

Klaus Jacobs

Laura Pirro

Loïc Eloi

Lucas Ivan Garbarino

Maria Herrero Manzano

Marie-Elisabeth Lissens

Nebojsa Korica

Noor Aljammal

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